

## Study of Carbonation-depth Prediction of Unsaturated Concrete Considering Carbonation-produced Water

Juan Long<sup>1)</sup>, Zhigao Peng<sup>2)\*</sup>, Haoxiong Feng<sup>3)</sup> and Aocheng Yang<sup>4)</sup>

<sup>1)</sup> School of Humanities, Hunan City University, Yiyang 413000, China.  
E-Mail: longjuan1225@sina.com

<sup>2)</sup> College of Civil Engineering, Hunan City University, Yiyang 413000, China  
\* Corresponding Author. E-Mail: pengzhgg@163.com

<sup>3)</sup> College of Civil Engineering, Hunan City University, Yiyang 413000, China.  
E-Mail: fenghaoxiong@hncu.edu.cn

<sup>4)</sup> College of Civil Engineering, Hunan City University, Yiyang 413000, China.  
E-Mail: yac2947583035@163.com

### ABSTRACT

Carbon dioxide can react with alkaline carbonate substances in cement-based materials, which harms the durability of the concrete structure. The carbonation reaction is a process of releasing water, resulting in an increase in pore water saturation, which was always neglected by previous studies. In this paper, a transient pore water saturation equation is proposed and introduced into the classical carbonation reaction kinetic model, which is simulated by finite-element software with a typical ordinary Portland cement. The model was verified by two classical empirical equations for carbonation-depth prediction. The simulation results indicated that the increment of pore water saturation originated by carbonation-produced water will weaken the CO<sub>2</sub> diffusivity and enhance the carbonation resistance. Besides, the growth rate of carbonation depth is slightly faster without considering the produced water and with higher initial saturation, the difference will be more significant. If the influence of carbonation water is ignored, the predicted carbonation depth of unsaturated concrete may be less accurate.

This study can provide some reference for theoretical and experimental studies on concrete carbonation. However, future work is still needed including more realistic effects in the model such as the mesoscale modeling of concrete and the integration of stress states.

**KEYWORDS:** Ordinary Portland concrete, Carbonization reaction, Carbon-dioxide transport, Finite-element method, Pore saturation.

### INTRODUCTION

The basic constituent materials of concrete are cement, water, sand and aggregates. Generally, the liquid phase inside the concrete is strongly alkaline. Under this condition, a dense passivation film is formed on the surface of the reinforcing steel in concrete to protect it from corrosion (Chen et al., 2019). However, due to the evaporation of water in the hardening process of concrete, a large number of pores are formed (Wang

et al., 2019). Under the effect of concentration or pressure gradient, carbon dioxide in the environment invades the concrete through these pores and reacts with alkaline carbonate substances in cement-based materials; i.e., carbonation reaction, resulting in the reduction of pH value in concrete (Sormeh et al., 2015). When the pH value of the cement-based materials around the rebar decreases from 12.5~13.0 to below 9.0, the passivation film on the surface of the rebar begins to activate until it disappears. Then, the rebar will corrode if sufficient water and oxygen are available. The corrosion and swelling of the reinforcement will make the passivation film spall, resulting in a reduction in the

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effective bearing area of the reinforcement and shortening the service life of reinforced concrete (Borg et al., 2017; Maekawa, 2008). Therefore, the resistance to carbonation is an important indicator of the durability of reinforced-concrete structures and is receiving increasing attention. The increase in CO<sub>2</sub> concentration will intensify the carbonation of concrete structures and bring more adverse effects on the durability of concrete structures (Sancheti et al., 2020; Wang et al., 2011). Monitoring results show that the concentration of CO<sub>2</sub> in the atmosphere has increased by 25% in the last century. The average concentration of CO<sub>2</sub> in the atmosphere was  $280 \times 10^{-6}$  kg/m<sup>3</sup> in the middle of the 19<sup>th</sup> century, reaching  $379 \times 10^{-6}$  kg/m<sup>3</sup> in 2005 and being expected to rise to  $1291 \times 10^{-6}$  kg/m<sup>3</sup> by 2100 (Yoon et al., 2007).

Carbonation is a complex physicochemical process in which atmospheric CO<sub>2</sub> penetrates the concrete. CO<sub>2</sub> is mainly diffused in the pore-fracture system of concrete and a classical theoretical model of concrete carbonation is derived from Fick's first law, which lays a foundation for future research (Thilakarathna et al., 2020). At present, carbonization models can be divided into four categories (Han, 2012): the first category is the theoretical carbonization model based on the Fick diffusion law and chemical reaction equation. Papadakis et al. (1989, 1991a; c) analyzed the process of carbonation reaction of concrete, studied the rate of cement hydration and carbonation using the method of chemical kinetics reaction and established a mathematical model in the form of a system of differential equations based on the mass balance condition of each carbonate compound in the carbonation process. Saetta et al. (1995) and Saetta and Vitaliani (2004, 2005) considered multi-factor correction including the moisture diffusion coefficient, heat transfer coefficient and chloride ion diffusion coefficient, introduced the source term of chemical reaction of carbonization with a multi-factor correction to the carbonization model and established the moisture-heat transfer-carbonization model. However, its deficiency is that the model parameters are not easily determined for engineering applications (Papadakis et al., 1989, 1991a; c). The second category is empirical carbonation models based on carbonation experiments; i.e., the rapid carbonation and natural carbonation experiments, where the model parameters are

determined from actual data. Numerous studies have shown that the depth of concrete carbonation is proportional to the square root of the carbonation time (Han, 2012). However, this type of model is proposed based on specific material components and environmental conditions and many empirical parameters have no specific physical significance and are not sufficiently generalized. The third category is the semi-theoretical and semi-empirical models based on both the theoretical models and experiments, which comprehensively analyze the principle of carbonation reaction and the influencing factors and determine the parameters in the theoretical model by experimental methods, having high practicality (Papadakis et al., 1991b). The fourth category is the stochastic prediction model of carbonation depth, which is a multi-coefficient stochastic model under the consideration of the variability of the concrete itself and the variability of the environment. However, such models are still in the primary research stage (Ruan, 2018; Thilakarathna et al., 2020; You et al., 2022).

The carbonation rate of ordinary Portland cement (OPC) is greatly influenced by the pore water saturation of concrete, due to that CO<sub>2</sub> transport and carbonation reactions are both related to the concrete pore space (Wang et al., 2019). When the pore saturation is small, the water content in the pore space is low and the CO<sub>2</sub> diffusivity is high. However, the carbonation rate is slower under this condition, because the required water (solvent) for carbonation reaction is insufficient. When the saturation is larger, the water fills the pore space and hinders the diffusion of CO<sub>2</sub>, also resulting in a slower carbonation rate (Anstice et al., 2005). What's more, the carbonation reaction itself is also a process of water release and the produced water will fill the concrete pore space and increase the pore saturation, which in turn affects the carbonation reaction. These inner effects were always neglected in previous studies. Therefore, in this paper, a transient pore saturation model is introduced into the kinetic equation of carbonation reaction to consider the influence of produced water on the kinetic process of carbonation reaction.

### **Effect of Water Produced by Carbonation Reaction on Pore Saturation**

The initial pore water saturation of concrete is affected by the environmental relative humidity, which

affects the carbonation efficiency. The water produced by the carbonation reaction will lead to an increase in saturation and the transient pore water saturation can be obtained from Eqs. (1)~(3).

$$s = s_0 + \Delta s = \frac{V_w}{V_v} + \frac{V_{wp}}{V_v} \quad (1)$$

$$V_{wp} = \frac{m_w}{\rho_w} = \frac{n_{H_2O} \cdot M_{H_2O}}{\rho_w} = \frac{c_{H_2O} \cdot V_w \cdot M_{H_2O}}{\rho_w} \quad (2)$$

$$\Delta s = \frac{V_{wp}}{V_v} = \frac{V_w}{V_v} \frac{V_{wp}}{V_w} = s_0 \cdot \frac{c_{H_2O} M_{H_2O}}{\rho_w} \quad (3)$$

where  $s_0$  is the initial saturation of concrete, %;  $\Delta s$  is the saturation variation caused by produced water, %;  $V_w$  and  $V_{wp}$  are the initial and produced water contents

in the pores, respectively,  $m^3$ ;  $V_v$  is the total volume of the pores,  $m^3$ ;  $c_{H_2O}$  is the concentration of the produced water,  $mol/m^3$ .

The model can adaptively adjust the variation of pore saturation according to the amount of water produced by carbonation at each instant; however, the effect of the produced water content on the concentration of each substance is not considered, for the sake of computational simplicity. Figure 1 shows the variation of pore saturation caused by the reaction that produced water at different initial saturations. It is suggested that the water produced by the carbonation reaction with a high level of the initial saturation will significantly increase the pore saturation and the results obtained may be inaccurate if the amount of produced water is not considered in the carbonation reaction.

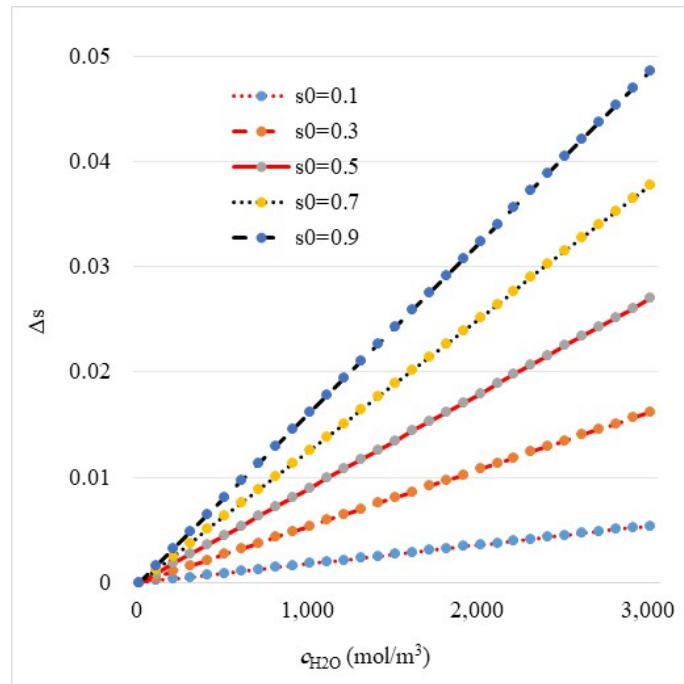


Figure (1): Variation of pore saturation caused by the amount of water produced by the carbonation reaction at different porosities

## RESULTS AND DISCUSSION

### Initial and Boundary Conditions

In this paper, the finite-element software COMSOL Multiphysics is employed to simulate the kinetic process of concrete carbonation, in which the diffusion reaction of each component involved in the reaction is governed by the coefficient partial differential-equation module.

The initial and boundary conditions are set as follows:

$$c_{CO_2} | (x, 0) = c_{CaCO_3} | (x, 0) = 0$$

$$c_{CH} | (x, 0) = 2694.6(mol / m^3)$$

$$c_{CSH} | (x, 0) = 345.6(mol / m^3)$$

$$c_{CO_2} | (0, t) = 10\%$$

$$\mathbf{n} \cdot (D_i \nabla c_i) = 0$$

Other parameters can be seen in Table 1.

**Table 1. The input parameters for COMSOL simulation**

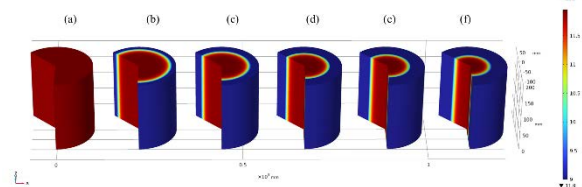
Parameters	Quantities
Initial pore water saturation $s_0$ (%)	65, 75
Water-cement ratio $R_{w/c}$	0.5, 0.6, 0.7
Aggregate-cement ratio $R_{a/c}$	4
Temperature $T_0$ (°C)	20
Dissolution of CH $\mu$	0.165
Initial diffusion coefficient of $CO_2$ $D_{0,CO_2}$ ( $m^2/s$ )	$1.64 \times 10^{-6}$
Diffusion coefficient of CH $D_{CH}$ ( $m^2/s$ )	$1.00 \times 10^{-12}$
Diffusion coefficient of CSH $D_{CSH}$ ( $m^2/s$ )	$1.00 \times 10^{-12}$
Diffusion coefficient of $H_2O$ $D_{H_2O}$ ( $m^2/s$ )	$1.00 \times 10^{-11}$
Diffusion coefficient of $CaCO_3$ $D_{CaCO_3}$ ( $m^2/s$ )	$1.00 \times 10^{-12}$
Reaction constant of CH $K_{CH}$ [ $m^3/(mol*s)$ ]	$5.0 \times 10^{-6}$
Reaction constant of CSH $K_{CSH}$ [ $m^3/(mol*s)$ ]	$3.9 \times 10^{-8}$
Water density $\rho_w$ ( $kg/m^3$ )	1000
Concrete density $\rho_c$ ( $kg/m^3$ )	3100
Aggregate density $\rho_a$ ( $kg/m^3$ )	2800

### Effect of Pore Water Saturation and Water-Cement Ratio on Carbonation Depth

Figure 2 shows the variation of carbonation depth of concrete with time for the initial percentage of  $CO_2$   $[CO_2]^0=10\%$ , initial pore water saturation  $s_0=65\%$  and water-cement ratio  $R_{w/c}=0.6$ . It can be found that the initial carbonation depth is 0. There are three regions of complete carbonation (blue), partial carbonation (yellow) and uncarbonated (red) when carbonation depth increases with time. After 500 days, the carbonation depth is 42.8 mm when the amount of produced water in the carbonation reaction is considered, which reached 45.4 mm when ignoring the influence of produced water.

Figure 3 shows the carbonation depths at different  $s_0$  and  $R_{w/c}$  and the results are compared with those of two classical empirical carbonation depth prediction models of Papadakis et al. (1991a) and Zhang and Jiang (1998), respectively. The results in Figs. 3 (a)~(c) and (d)~(f) show that the carbonation depth grows faster with larger  $w/c$  for the same  $s_0$ . This is because the carbonation reaction depends not only on the amount of cement hydration product CH, but also on the diffusion of  $CO_2$  into the concrete interior, both of which are very closely related to the water-cement ratio. When other conditions are the same only the water-cement ratio is different, the amount of CH generated by hydration is the same and

the diffusivity of  $CO_2$  is dominant in the carbonation resistance of concrete. Under these conditions, a larger water-cement ratio will result in more pores in the internal structure of the concrete, making the concrete less dense and  $CO_2$  easier to diffuse, which accelerates the carbonation rate. Comparing the simulation results with those of these two empirical models, it can be found that the results of both two cases are between these two empirical models and are more consistent with the results predicted by Zhang and Jiang (1998), which suggest that the accuracy of our model is sufficient to predict the carbonization depth. Besides, the growth rate of carbonation depth is slightly faster when the effect of produced water of carbonation reaction on the carbonation kinetic process (the marks of  $s_0$ ) is neglected and with higher initial saturation, the difference between the two cases will be larger, which agrees well with the prediction of our model in Fig. 1.



**Figure (2): Variation of carbonization depth with time. (a)  $t=0d$ , (b)  $t=100d$ , (c)  $t=200d$ , (d)  $t=300d$ , (e)  $t=400d$ , (f)  $t=500d$**

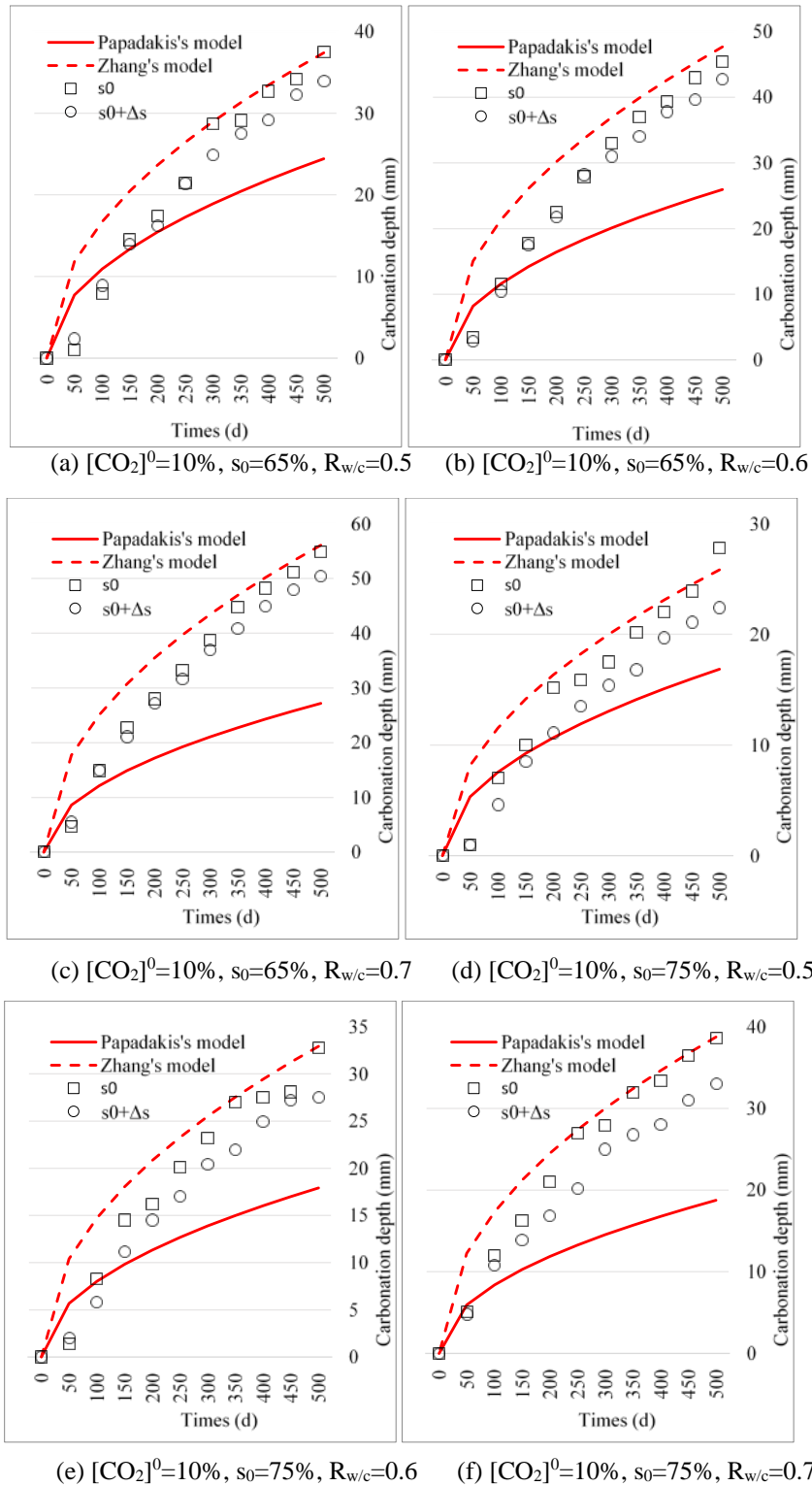


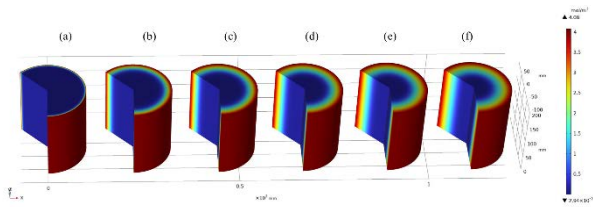
Figure (3): Carbonization depth under different water saturation and water-cement ratio

**Characteristics of Distribution of Each Component Concentration during Carbonation Reaction**

The carbonation reaction is directly related to the

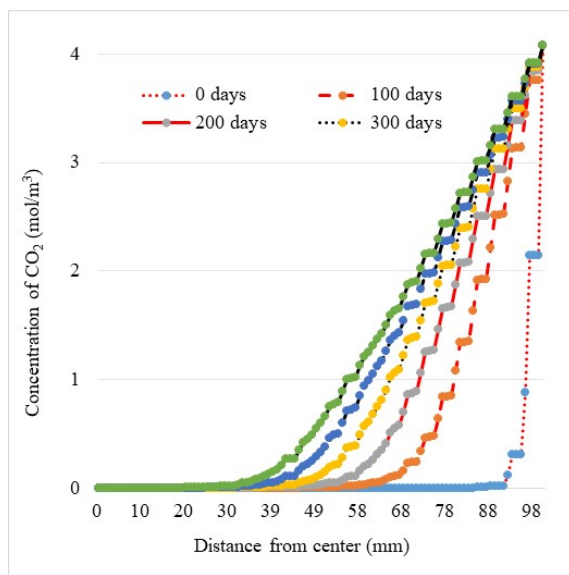
concentration magnitude and distribution of  $\text{CO}_2$ . The environmental concentration of  $\text{CO}_2$  in this paper is 10%, which is converted into  $4.076 \text{ mol/m}^3$ . The  $\text{CO}_2$  is

driven by the concentration gradient to transfer to the inner part of the concrete along the carbonation path and carbonize with CH and CSH. The process is shown in Fig. 4.

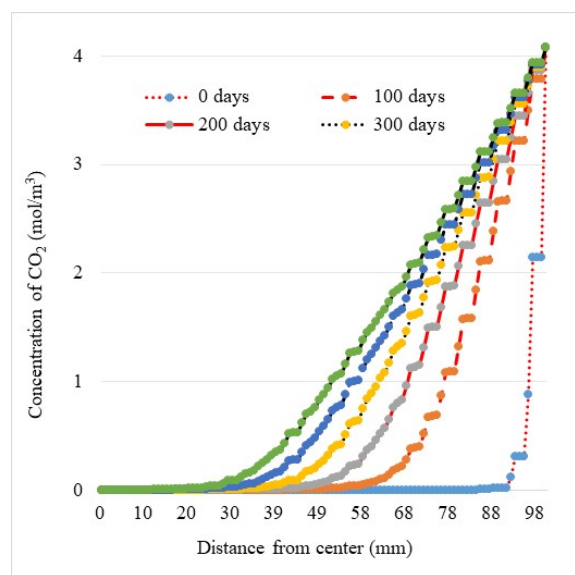


**Figure (4): Distribution of CO<sub>2</sub> concentration at different times. (a) t=0d, (b) t=100d, (c) t=200d, (d) t=300d, (e) t=400d and (f) t=500d**

Figure 5 shows the magnitude and distribution of CO<sub>2</sub> concentration at different times. It can be observed that the CO<sub>2</sub> concentration in the carbonation-reaction zone gradually increases with time, but the growth rate becomes smaller and smaller, indicating that the carbonation resistance becomes larger with increasing the carbonation depth. When the effect of carbonation-produced water is considered, both the magnitude of CO<sub>2</sub> concentration and the concentration increments along the carbonation direction over time are significantly smaller than the results of neglecting produced water, due to the increase of the pore water saturation, which weakens the CO<sub>2</sub> diffusivity.



(a)



(b)

**Figure (5): The magnitude and distribution of CO<sub>2</sub> concentration at different times. (a) without considering the effect of produced water and (b) considering the effect of produced water**

Figure 6 shows the magnitude and distribution of the concentration of H<sub>2</sub>O produced by the carbonation reaction at different times. Before the reaction, the H<sub>2</sub>O content is 0. After 100 days of carbonization, the carbonation reaction with CH and CSH occurs after the outside CO<sub>2</sub> is transferred into concrete, rapidly consuming the local concentration of CH and CSH. The H<sub>2</sub>O concentration in the fully carbonated zone reaches the maximum value of 2440.28 mol/m<sup>3</sup>, which gradually decreases along the carbonation direction as the carbonation continues, the front line of produced H<sub>2</sub>O concentration gradually moves forward along the

carbonation direction with the carbonation reaction zone. Combined with the results of Fig.1, it can be seen that the concentration of produced H<sub>2</sub>O has some increment in water saturation during carbonation.

Figure 7 summarizes the concentration magnitude and distribution of each reactant and product along the carbonation direction. It can be found that the initial content of CH is larger and the reaction rate with CO<sub>2</sub> is faster than that of CSH, which is rapidly consumed by CO<sub>2</sub> in the carbonation reaction zone and its content decreases sharply. The variation of CSH is similar to that of CH, but the consumption rate is slower due to its

initial content being smaller and the reaction rate with CO<sub>2</sub> being lower.

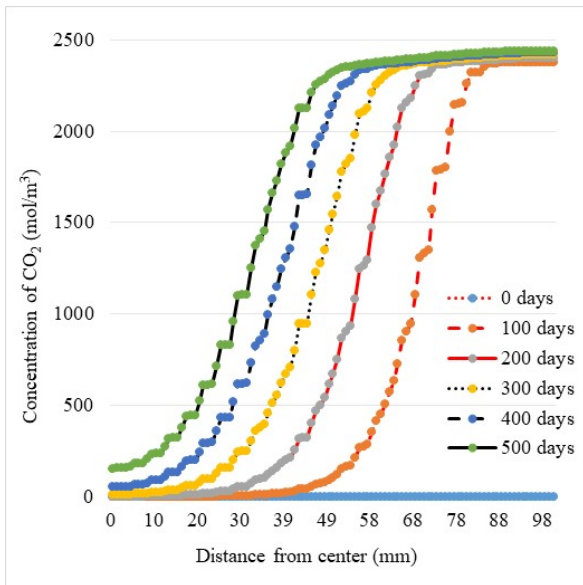


Figure (6): The magnitude and distribution of H<sub>2</sub>O concentration at different times

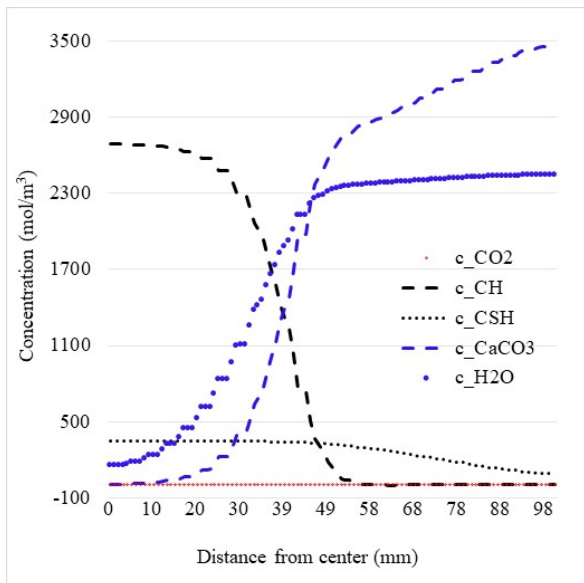


Figure (7): Concentration distribution of each component substance at 500 days

The main component of the uncarbonated zone is CH, while the main component of the complete carbonated zone is CaCO<sub>3</sub>. In the carbonation reaction zone, the CaCO<sub>3</sub> content gradually increases and the CH content gradually decreases along the carbonation direction. After 500 days of carbonation, the concentration of H<sub>2</sub>O in the fully carbonated zone is much lower than that of CaCO<sub>3</sub>, while in the carbonation

reaction zone and the uncarbonated zone, the concentration of H<sub>2</sub>O is slightly higher than that of CaCO<sub>3</sub>. This is because the reaction of CO<sub>2</sub> and CSH is slower than that of CH and the concentration of CaCO<sub>3</sub> produced in the later stage is greater than that of H<sub>2</sub>O. Moreover, the diffusivity of H<sub>2</sub>O in concrete is much greater than that of CaCO<sub>3</sub> and the H<sub>2</sub>O in the fully carbonated zone will be driven by the concentration difference to diffuse to the carbonation reaction area and the uncarbonated area. This difference is smaller in the early stage of the carbonation reaction and becomes larger and larger as carbonation proceeds.

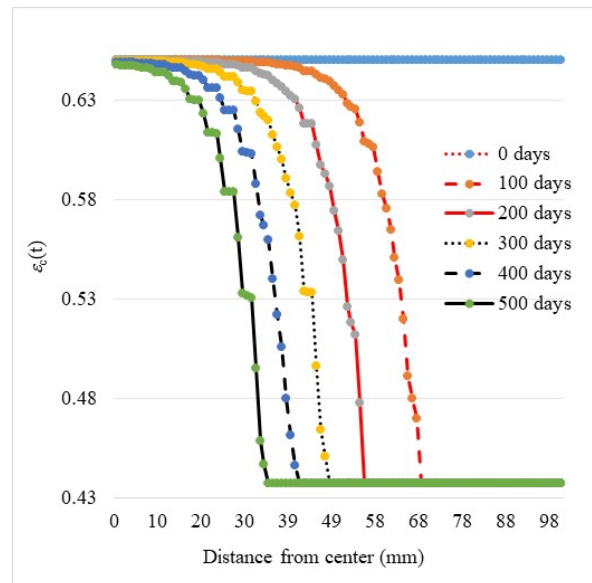


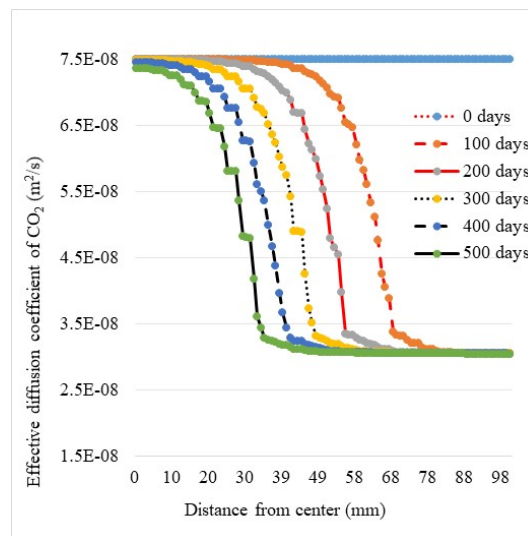
Figure (8): The variation of porosity during the carbonation reaction

**The Variation of Porosity and CO<sub>2</sub> Diffusivity during Carbonation Reaction**

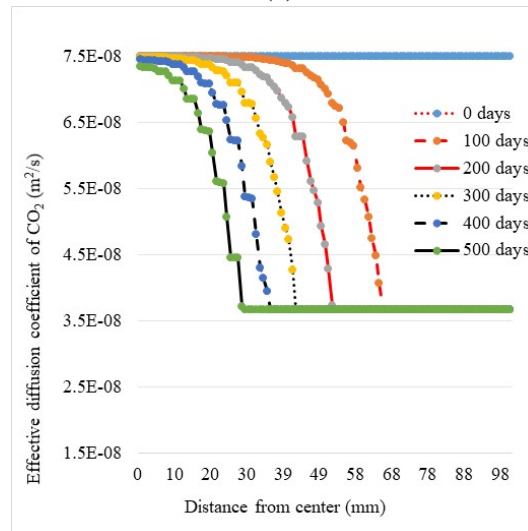
Porosity is an important factor affecting the carbonation of concrete, because it directly affects the diffusivity of carbon dioxide. Figure 8 shows the variation of porosity during the carbonation reaction. It can be observed that the initial porosity of the concrete is 0.65 after considering the amplification effect of porosity in the interface transition zone (ITZ), while porosity decreases with time in the carbonation-reaction zone and drops to the lowest point of 0.44 in the fully carbonated zone. The porosity of cementitious composites is closely related to the water-cement ratio ( $R_{w/c}$ ) where higher  $R_{w/c}$  leads to an increase in porosity and promotes CO<sub>2</sub> diffusivity, which increases the degree of carbonation. Therefore, the degree of

carbonation usually increases with  $R_{w/c}$ . However, as  $R_{w/c}$  increases to the limit, the degree of carbonation will not increase further due to the decrease in the amount of cement and this conclusion has also been confirmed by literature (Wang et al., 2019). According to the model proposed by Chen et al. (2019) and Papadakis et al. (1991a), the change in porosity is proportional to the difference in molar volume between the solid reactants and the solid products. Houst and Wittmann (1994), using numerical models and experimental measurements, found that the effective diffusivity increases exponentially with increasing porosity.

Generally, the water produced by the carbonation reaction does not change the porosity of the concrete, but the effect on the pore saturation will change the  $\text{CO}_2$  transport efficiency. Figure 9 shows the variation of the effective diffusion coefficient of  $\text{CO}_2$  during carbonation in the two cases, respectively. It can be found that the influence of carbonation kinetics on  $\text{CO}_2$  diffusivity is greater when the effect of produced water is considered and the effective diffusion coefficient of  $\text{CO}_2$  in the fully carbonated zone decays more, which will cause more "resistance" to the carbonation process in the carbonation-reaction zone.



(a)



(b)

**Figure (9): The variation of  $\text{CO}_2$  diffusivity during carbonation reaction.**  
**(a) considering the effect of produced water and**  
**(b) without considering the effect of produced water**



## CONCLUSIONS

In this paper, a transient pore saturation model is introduced into the carbonation reaction kinetic model to consider the influence of produced water on the process of carbonation reaction. The finite-element software COMSOL Multiphysics is employed to simulate the kinetic process of concrete carbonation, in which the diffusion reaction of each component involved in the reaction is governed by the coefficient partial differential-equation module and the physicochemical parameters involved were estimated using empirical equations. The effect of carbonation-produced water on the reaction kinetic process was analyzed and the results were compared with those of two classical empirical carbonation models. The conclusions were as follows:

1. The comparison relationship between the simulation results and these two empirical models suggests that the accuracy of our model is sufficient to predict the carbonization depth.
2. The growth rate of carbonation depth is slightly faster when the effect of produced water of carbonation reaction on the carbonation kinetic process is neglected and with higher initial saturation, the difference between the two cases will be larger, which agrees well with the prediction of our model.
3. Carbonation resistance increases with carbonation depth and the carbonation-produced water will further enhance the resistance, especially in the fully carbonated zone, due to that the increase of the pore water saturation weakens the effective CO<sub>2</sub> diffusivity.
4. In the process of unsaturated concrete carbonation, a large amount of water has been produced during carbonization. In our cases, the carbonation-produced water in the fully carbonated zone reaches the maximum value of 2440.28 mol/m<sup>3</sup>, which will significantly increase the pore water saturation. When predicting the carbonation depth of unsaturated concrete, if the influence of carbonation water is ignored, the results may be less accurate.

The methods and results of this study can provide some reference for theoretical and experimental studies on concrete carbonation. However, future work is still needed including more realistic effects in the model, such as the mesoscale modeling of concrete and the integration of stress states.

### Data Availability

The data used to support the findings of this study is included in the article.

### Conflicts of Interest

The authors declare that they have no conflicts of interest.

### Acknowledgments

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### Supplementary Materials

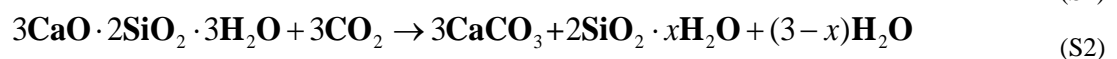
This part contains two sections. The details of modeling the concrete carbonation process are stated in Sec. S1, while the description of parameters in the simulation is shown in Sec. S2.

### Supplementary Material

#### S1. Modeling of the Concrete Carbonation Process

##### S1.1 Simplified Model of Concrete Carbonation

The carbonate component in concrete is mainly Ca(OH)<sub>2</sub> (hereafter referred to as CH), hydrated calcium silicate (3CaO·2SiO<sub>2</sub>·3H<sub>2</sub>O, CSH), un-hydrated tricalcium silicate (3CaO·SiO<sub>2</sub>, C3S) and dicalcium silicate (2CaO·SiO<sub>2</sub>, C2S) in the presence of water. The concrete carbonization process mainly involves the following four chemical reactions:



Generally, the value of x in Equation (S2) is 2.5

(Maekawa, 2008: 241). According to the research of

Papadakis et al. (1989), the content of C3S and C2S in the OPC is very small and has a limited effect on the whole carbonation process (Papadakis et al. 1991a). Therefore, in this paper, we only consider the chemical reactions between CH, CSH and CO<sub>2</sub>. Based on the law of conservation of substances' mass, the evolution equation for the substances' transport of each component in the carbonization process can be obtained (Maekawa, 2008) from Eq. (S5).

$$\frac{\partial C_i}{\partial t} = D_i \nabla^2 C_i + R_i \quad (S5)$$

where  $C_i$  is the concentration of each component, mol/m<sup>3</sup>;  $D_i$  is the corresponding diffusion coefficient, m<sup>2</sup>/s;  $R_i$  is the source/sink term.

### S1.2 CO<sub>2</sub> Transport in Concrete

The CO<sub>2</sub> diffusion coefficient in concrete cannot be derived from experiments due to the carbonation reaction between CO<sub>2</sub> and cement, resulting in inaccurate test results, which are generally obtained by multiplying the transport coefficient of nitrogen or oxygen in concrete by the molar mass ratio of nitrogen or oxygen to CO<sub>2</sub>. Papadakis (Millington, 1959) considered the effect of porosity and pore saturation and proposed the effective diffusion coefficient of CO<sub>2</sub> in concrete as in Eq. (S6).

$$D_{CO_2} = 1.64 \times 10^{-6} \cdot \phi^{1.8} (1-s)^{2.2} \quad (S6)$$

where  $\phi$  is the porosity of concrete;  $s$  is the saturation of pores in concrete.

### S1.3 Carbonization Reaction Rate

The carbonation simulation results of Du (2009) show that the effect of the concrete pore solution saturation should be considered in the CH carbonation reaction constant  $K_{CH}$  under the partially saturated state as in Eq. (S7).

$$K_{CH} = K_{CH}^0 \times s^{3.7} \quad (S7)$$

The simulation results of Park (2008) show that initial carbonation reaction constants  $K_{CH}^0$  of CH under the saturated state ranged from  $5 \times 10^{-6}$  to  $5 \times 10^{-4}$ . According to the results of thermo-gravimetric analysis (TGA) from Papadakis et al. (1989),

$$\frac{K_{CSH}}{K_{CH}} = 7.8 \times 10^{-3} \quad (S8)$$

Therefore, the carbonation reaction rates of CH and CSH can be obtained from Eqs. (S9) and (S10).

$$R_{CH} = -\varepsilon_c(t) \times k_{CH} \times s^{3.7} \times c_{CO_2} \times c_{CH} \quad (S9)$$

$$R_{CSH} = -k_{CSH} \times s^{3.7} \times c_{CO_2} \times c_{CSH} \quad (S10)$$

### S1.4 Variation of Concrete Porosity during Carbonization

The carbonation reaction in the OPC leads to a decrease in total porosity, because the volume of the product (i.e., CaCO<sub>3</sub>) is higher than that of the main reactant i.e., CH (Bogue, 2008; Camilleri, 2007). Papadakis et al. (1989, 1991b) proposed Eq. (S11) for estimating the initial porosity of cement.

$$\varepsilon_0 = \frac{R_{w/c} \times \frac{\rho_c}{\rho_w}}{\left( R_{w/c} \times \frac{\rho_c}{\rho_w} + R_{a/c} \times \frac{\rho_c}{\rho_a} + 1 \right)} \quad (S11)$$

where  $\rho_c$ ,  $\rho_w$  and  $\rho_a$  are the density of concrete, water and aggregate, respectively, kg/m<sup>3</sup>;  $R_{w/c}$  is the water-cement ratio;  $R_{a/c}$  is the aggregate-cement mass ratio.

Due to the presence of pores in the interface transition zone (ITZ) between the cement paste and the aggregates, an amplification factor  $\eta_0$  in the porosity of concrete should be taken into consideration (Burkan Isgor and Razaqpur, 2004; Papadakis et al., 1991b).

$$\eta_0 = \left( 1 + \frac{R_{a/c} \times \frac{\rho_c}{\rho_a}}{1 + R_{w/c} \times \frac{\rho_c}{\rho_w}} \right) \quad (S12)$$

Therefore, the porosity of the concrete before the start of the carbonation reaction can be obtained from Eq. (S13).

$$\varepsilon = \varepsilon_0 \eta_0 \quad (S13)$$

Ishida et al. (Van Belleghem et al., 2014; Zhang and Lounis, 2006) assumed that the distribution of pore size would not change during the carbonation reaction, only

considering the decrease of porosity. They established the linear functional relationship between the decrease of porosity and the residual amount of calcium hydroxide and water-cement ratio as in Eqs. (S14) and (S15).

$$\begin{cases} \varepsilon_c(t) = \alpha \cdot \varepsilon \\ \alpha = \alpha_f \quad (R < \beta) \\ \alpha = 1.25 \cdot R - 0.25 \quad (\beta < R, 1) \end{cases} \quad (S14)$$

$$\begin{cases} \alpha_f = 0.67 \cdot R_{w/c} + 0.27 \\ \beta = 0.8 \cdot \alpha_f + 0.2 \end{cases} \quad (S15)$$

where  $\varepsilon_c$  is the porosity during the carbonation reaction;  $\alpha$  and  $\alpha_f$  are the degrees of porosity reduction;  $R$  is the ratio of the amount of consumed calcium hydroxide to the overall calcium hydroxide.

### S1.5 Carbonation Depth Estimation Method

To deeply understand the kinetics of concrete carbonation, a large number of studies involving model-based simulation and laboratory experiments have been carried out (Hyvert et al., 2010; Sisomphon and Franke, 2007). The natural carbonation process of cementitious materials is very slow and may last for decades. Therefore, the accelerated carbonation method is proposed to evaluate the carbonation resistance of cementitious materials in a short period using a higher concentration of  $CO_2$ . The most general, simplified and widely used expression for predicting the carbonation depth of cement-based materials can be obtained from Eq. (S16) (Guiglia and Taliano, 2013; Houst and Wittmann, 2002; Siriwardena and Peethamparan, 2015).

$$x = b\sqrt{t} \quad (S16)$$

where  $x$  is the carbonation depth at  $t$  days;  $t$  is the carbonation exposure time;  $b$  is an empirical constant.

Houst and Wittmann (2002) pointed out that the derivation of Eq. (S15) is based on the assumption of a constant  $CO_2$  diffusivity. However, the  $CO_2$  diffusivity

varies with a lot of factors, including the degree of hydration, porosity,  $CO_2$  concentration, pore water saturation and the number and type of microscopic phases. Therefore, considering the micro-structural characteristics of OPC-based concrete systems, a more accurate physical model was developed to predict the carbonation rate of cementitious materials (Bary and Mügler, 2006; Bary and Sellier, 2004; Papadakis et al., 1991a). Papadakis et al. (1991a) proposed a theoretical model to predict the depth of carbonation:

$$x = \sqrt{\frac{2D_{e,CO_2} ([CO_2]^0 / 100)}{0.33c_{0,CH} + 0.214c_{0,CSH}}} \cdot \sqrt{t} \quad (S17)$$

where  $D_{e,CO_2}$  is the effective diffusion coefficient of  $CO_2$ ;  $[CO_2]^0$  is the initial percentage of  $CO_2$ , %;  $c_{0,CH}$  and  $c_{0,CSH}$  are the initial concentrations of CH and CSH, respectively, mol/m<sup>3</sup>;  $t$  is the carbonation time, d.

Zhang and Jiang (1998) proposed a semi-theoretical and semi-empirical model, as follows:

$$x = 839(1-s)^{1.1} \sqrt{\frac{R_{w/c} - 0.34}{c_0} [CO_2]^0} \cdot \sqrt{t} \quad (S18)$$

where  $c_0$  is the cement content, kg/m<sup>3</sup>.

Generally, the theoretical model of carbonation reaction employs the pH value to estimate the carbonation depth and the pH value can be obtained from Eq. (S19).

$$pH = 14 + \lg(2 \times 10^{-3} [CH_{(aq)}]) \quad (S19)$$

The CH produced by hydration has two forms inside the concrete: solid and liquid, but only the liquid CH ( $CH_{(aq)}$ ) will carbonate with  $CO_2$ , so the dissolution ratio  $\beta_0$  of CH should be considered in the carbonation. The solubility  $\mu$  is shown in Table S.1, and the remaining solubility corresponding to temperature can be obtained using linear interpolation.

$$\begin{cases} [CH_{(aq)}] = \beta_0 \times [CH] \\ \beta_0 = \frac{\mu}{100} \end{cases} \quad (S20)$$

Table S1. Solubility  $\mu$  of CH at different temperatures

T (°C)	0	10	20	30	40	50	60	70
Components								
Ca(OH) <sub>2</sub>	0.185	0.176	0.165	0.153	0.141	0.138	0.116	0.106

Note: the value in the table is the mass of CH (g) dissolved in 100g of water.

Parrott and Killoh (1989) divided the carbonation process into three parts: the fully carbonated zone, the partial-carbonization zone (carbonation-reaction zone) and the uncarbonated zone. Generally, the region of pH=8.5~9.0 in concrete is identified as the completely carbonized zone, pH=9.0~12.5 as the partially carbonized zone and pH=12.5~13.0 as the uncarbonized zone (Conciatori et al., 2010; Papadakis et al., 1991a). In this paper, the position corresponding to pH=9.0 is taken as the depth of complete concrete carbonation.

## S2. Description of Parameters in the Simulation

Many physicochemical parameters of the components are usually difficult to measure directly and need to be estimated. Papadakis et al. (1991b) proposed an empirical formula to estimate the initial molar concentration of each component in cement before hydration after full mixing. Carmel (Jolicoeur and Simard, 1998) graphically expressed the proportional

relationship of each component of cement clinker. Bogue (2008) and Camilleri (2007) established an empirical formula to estimate the percentage of each mineral component of cement clinker to cement mass based on measured data. Papadakis et al. (1989, 1991b) proposed an equation for estimating the initial porosity of cement during initial hydration. Masuda and Tanano (1991) found experimentally that the hydration product CH content is about 30% of cement when hydration is complete. Based on this conclusion, Park (2008) obtained an estimation formula for the hydration product CH content. Liu (2005) found that the CSH content of concrete at complete hydration was about 60% of the cement mass.

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